

Computer aided design of extrusion forming tools

J. M. Nóbrega and O. S. Carneiro

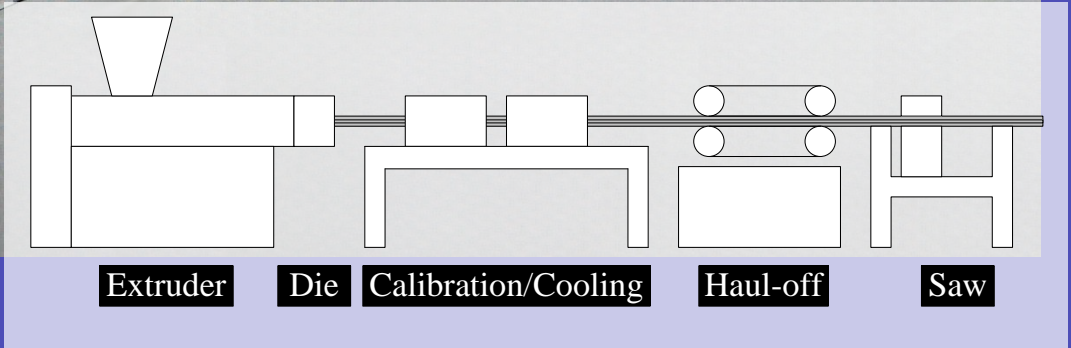
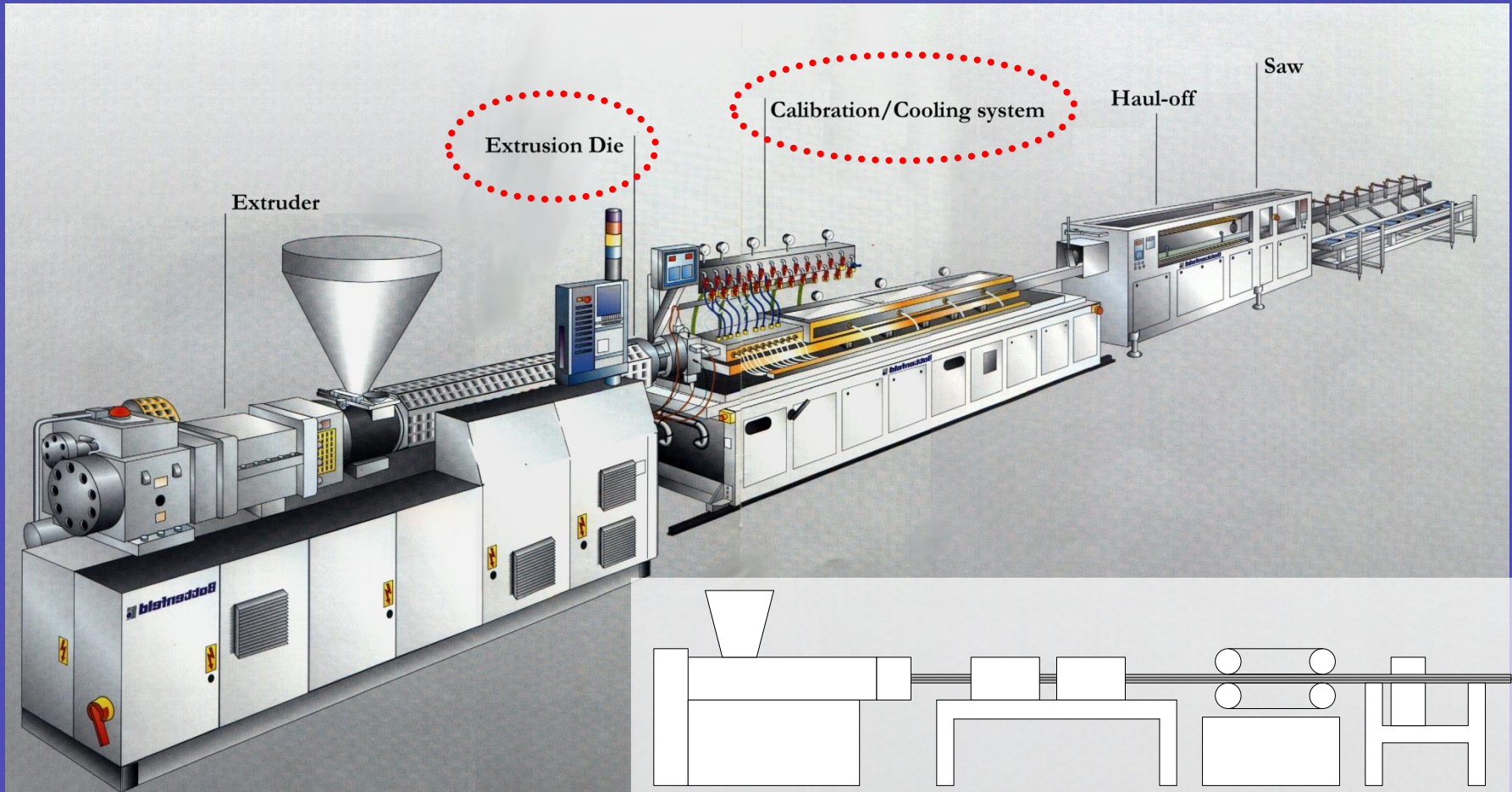


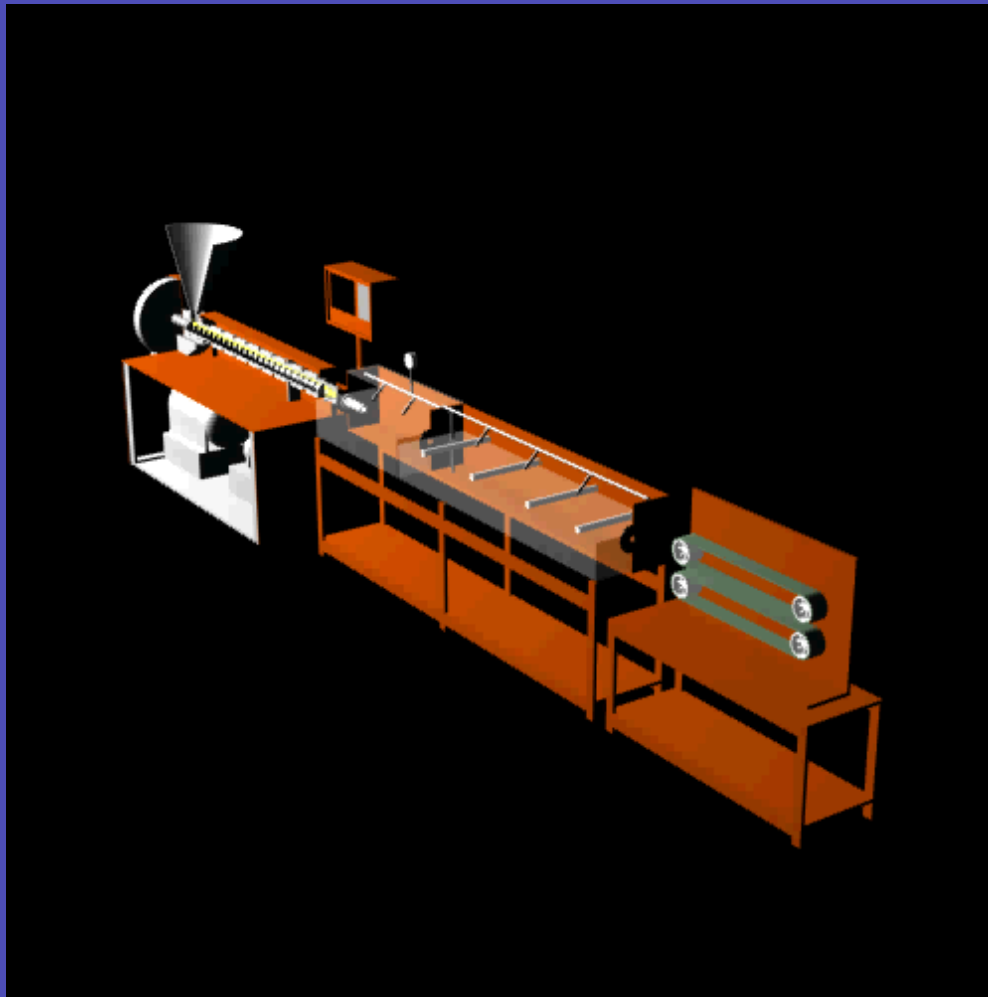
*I3N/IPC –Institute for Polymers and Composites
Department of Polymer Engineering
University of Minho
Portugal*

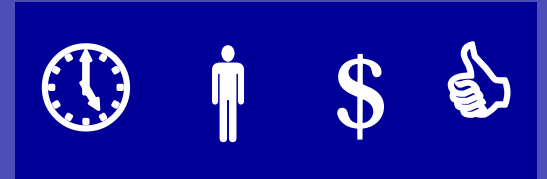


mnobrega@dep.uminho.pt / olgasc@dep.uminho.pt

Introduction - Profile Extrusion







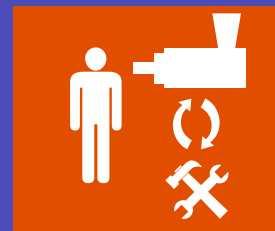
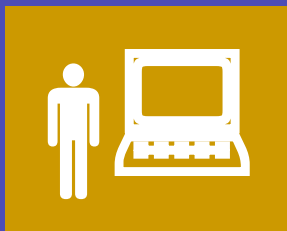
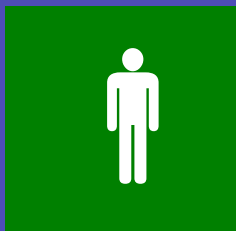
Traditional



Current



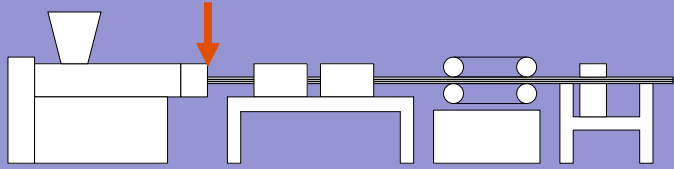
Under development





- **Extrusion Dies**
 - **Problem Statement**
 - **Flow Distribution Optimisation**
 - **Flow Balance Strategies**
 - **Optimisation**
 - **Length vs Thickness Optimisation**
 - **Conclusion**
- **Calibrators**
 - **Problem Statement**
 - **System Behaviour**
 - **Optimisation Methodology**
 - **Case Study**
 - **Conclusion**
- **Conclusion**
- **Ongoing Work**

Extrusion Dies – *Problem Statement*



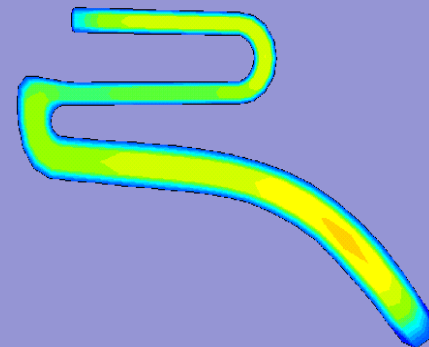
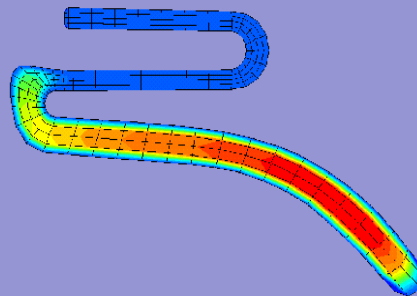
Unbalanced

Balanced

Extrusion run



**Numerical
Velocity contours**

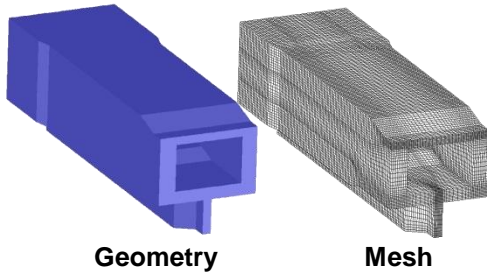


Extrusion Dies – Flow Distribution Optimisation



Trial Parameters

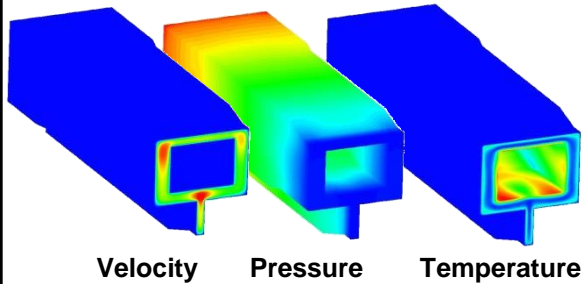
Pre-Processor



Geometry

Mesh

3D non-isothermal flow field calculation (FVM)



Velocity

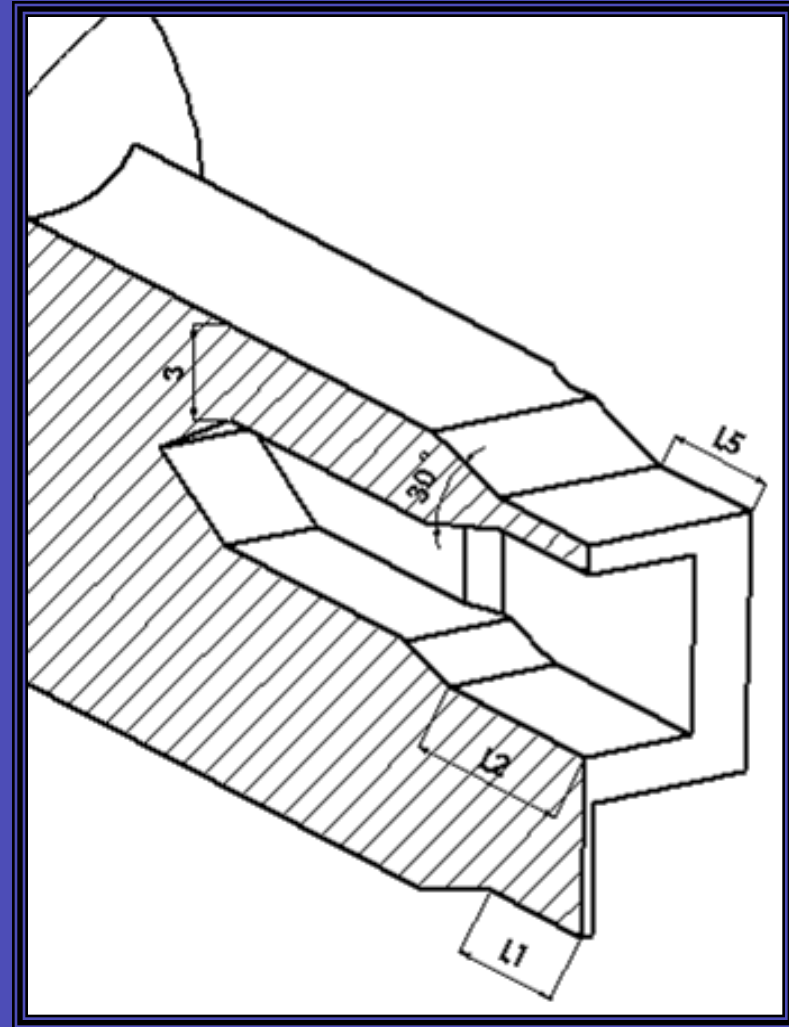
Pressure

Temperature

Performance Evaluation

$$F_{obj} = \sum_{i=1}^n \left\{ \left\{ \alpha \left(1 - \frac{V_i}{V_{obj,i}} \right)^2 + k(1-\alpha) \left[1 - \frac{(L/t)_i}{(L/t)_{min}} \right]^2 \right\} \frac{A_i}{A} \right\}$$

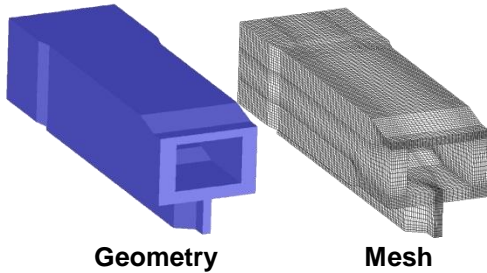
Modification of the controllable geometrical parameters until the optimum is reached





Trial Parameters

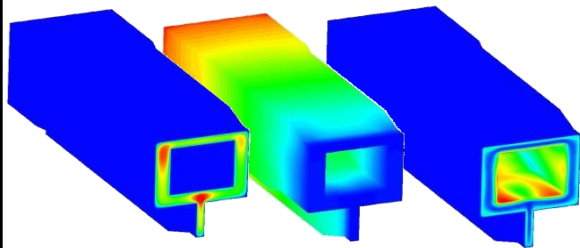
Pre-Processor



Geometry

Mesh

3D non-isothermal flow field calculation (FVM)



Velocity

Pressure

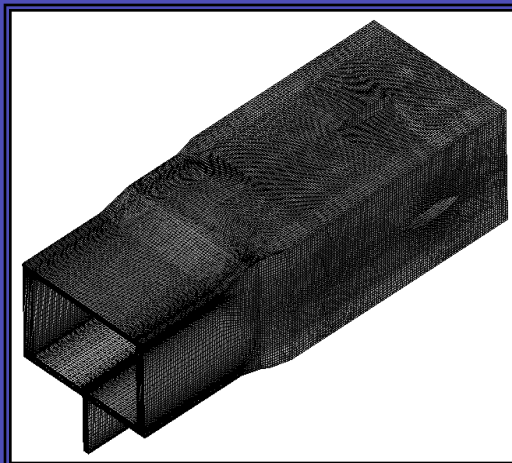
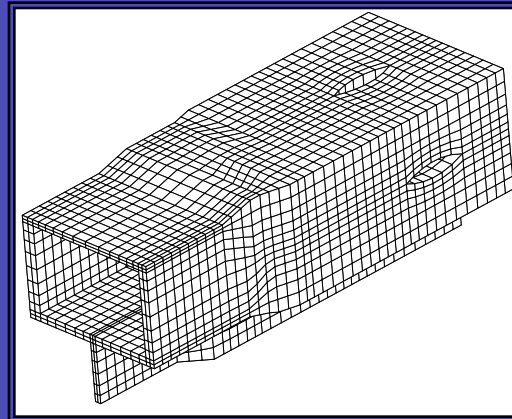
Temperature

Performance Evaluation

$$F_{obj} = \sum_{i=1}^n \left\{ \left\{ \alpha \left(1 - \frac{V_i}{V_{obj,i}} \right)^2 + k(1-\alpha) \left[1 - \frac{(L/t)_i}{(L/t)_{min}} \right]^2 \right\} \frac{A_i}{A} \right\}$$

Modification of the controllable geometrical parameters until the optimum is reached

Progressive mesh refinements



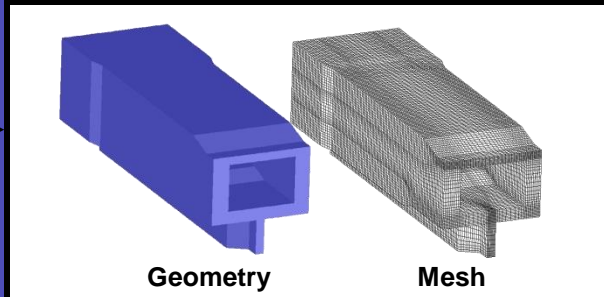
Cells along Thickness	Number of Cells	Time [h:m:s]
2	15 496	0:00:36
4	92 248	0:12:15
6	272 220	1:12:17
8	593 928	4:28:36
10	688 024	6:43:42

PIV / 2.4 GHz

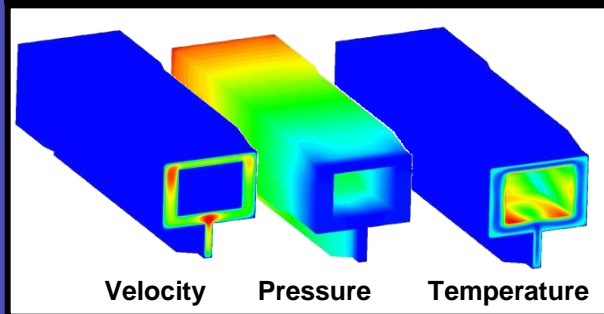


Trial Parameters

Pre-Processor



3D non-isothermal flow field calculation (FVM)



Performance Evaluation

$$F_{obj} = \sum_{i=1}^n \left\{ \left\{ \alpha \left(1 - \frac{V_i}{V_{obj,i}} \right)^2 + k(1-\alpha) \left[1 - \frac{(L/t)_i}{(L/t)_{min}} \right]^2 \right\} \frac{A_i}{A} \right\}$$

Modification of the controllable geometrical parameters until the optimum is reached

Equations to Solve

Conservation of mass:

$$\frac{\partial \rho u_j}{\partial x_j} = 0$$

Conservation of linear momentum:

$$\frac{\partial \rho u_i}{\partial t} + \frac{\partial \rho u_j u_i}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \frac{\partial \tau_{ij}}{\partial x_j}$$

Conservation of energy:

$$\frac{\partial \rho c T}{\partial t} + \frac{\partial \rho c u_i T}{\partial x_i} = \frac{\partial}{\partial x_i} \left(k \frac{\partial T}{\partial x_i} \right) + \tau_{ij} \frac{\partial u_i}{\partial x_j}$$

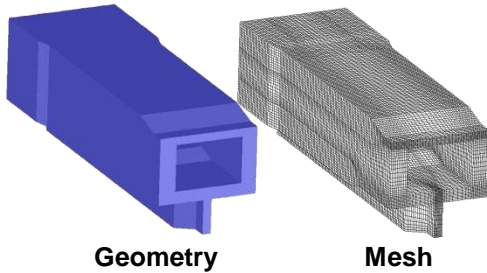
Constitutive equation (Gen. Newtonian):

$$\tau_{ij} = \eta(\dot{\gamma}) \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right)$$

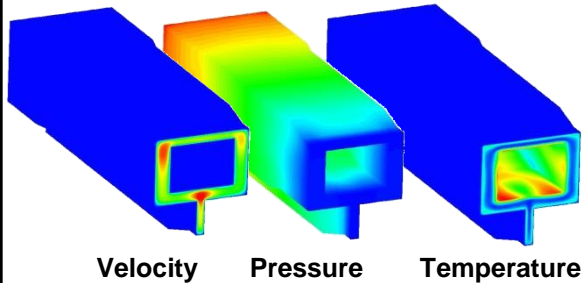


Trial Parameters

Pre-Processor



3D non-isothermal flow field calculation (FVM)



Performance Evaluation

$$F_{obj} = \sum_{i=1}^n \left\{ \left\{ \alpha \left(1 - \frac{V_i}{V_{obj,i}} \right)^2 + k(1-\alpha) \left[1 - \frac{(L/t)_i}{(L/t)_{min}} \right]^2 \right\} \frac{A_i}{A} \right\}$$

Modification of the controllable geometrical parameters until the optimum is reached

Equations to Solve

Conservation of mass:

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Conservation of linear momentum:

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Conservation of energy:

$$\frac{\partial \rho c T}{\partial t} + \frac{\partial \rho c u_i T}{\partial x_i} = \frac{\partial}{\partial x_i} \left(k \frac{\partial T}{\partial x_i} \right) + \tau_{ij} \frac{\partial u_i}{\partial x_j}$$

Constitutive equation (viscoelastic):

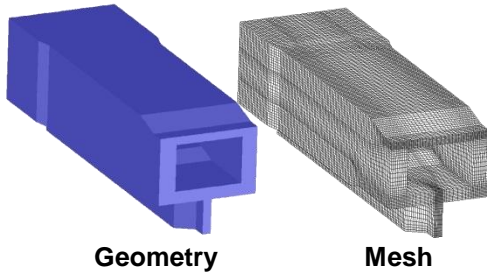
$$\tau_{ij} + \lambda \left(\frac{\partial \tau_{ij}}{\partial t} + \frac{\partial (u_k \tau_{ij})}{\partial x_k} \right) = \eta_p \left(\frac{\partial u_i}{\partial x_j} + \frac{\partial u_j}{\partial x_i} \right) + \lambda \left(\tau_{jk} \frac{\partial u_i}{\partial x_k} + \tau_{ik} \frac{\partial u_j}{\partial x_k} \right)$$

Extrusion Dies – Flow Distribution Optimisation

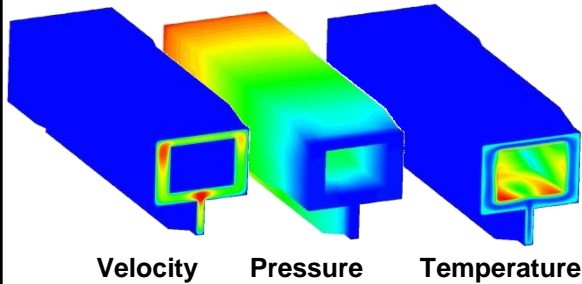


Trial Parameters

Pre-Processor



3D non-isothermal flow field calculation (FVM)



Performance Evaluation

$$F_{obj} = \sum_{i=1}^n \left\{ \left\{ \alpha \left(1 - \frac{V_i}{V_{obj,i}} \right)^2 + k(1-\alpha) \left[1 - \frac{(L/t)_i}{(L/t)_{min}} \right]^2 \right\} \frac{A_i}{A} \right\}$$

Modification of the controllable geometrical parameters until the optimum is reached

Objective Function

Area Weighting

$$F_{obj} = \sum_{i=1}^n \left\{ \left\{ \alpha \left(1 - \frac{V_i}{V_{obj,i}} \right)^2 + k(1-\alpha) \left[1 - \frac{(L/t)_i}{(L/t)_{min}} \right]^2 \right\} \frac{A_i}{A} \right\}$$

Flow Balance

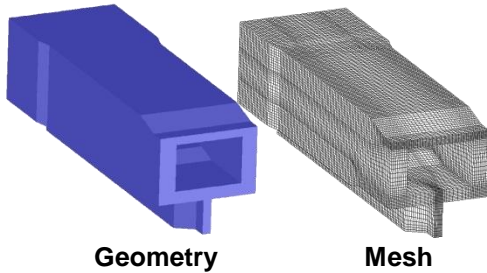
Admissible L/t value

Area Weighting

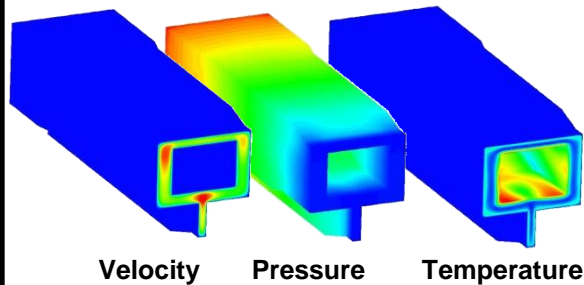


Trial Parameters

Pre-Processor



3D non-isothermal flow field calculation (FVM)



Performance Evaluation

$$F_{obj} = \sum_{i=1}^n \left\{ \left\{ \alpha \left(1 - \frac{V_i}{V_{obj,i}} \right)^2 + k(1-\alpha) \left[1 - \frac{(L/t)_i}{(L/t)_{min}} \right]^2 \right\} \frac{A_i}{A} \right\}$$

Modification of the controllable geometrical parameters until the optimum is reached

SIMPLEX Method (SM)

Experimental Method (EM)

Extrusion Dies – Flow Balance Strategies



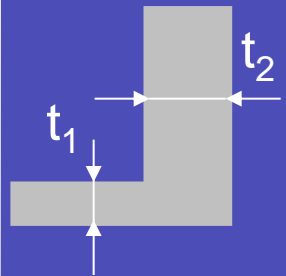
Required Profile

Optimised Variable

Die Flow Channel

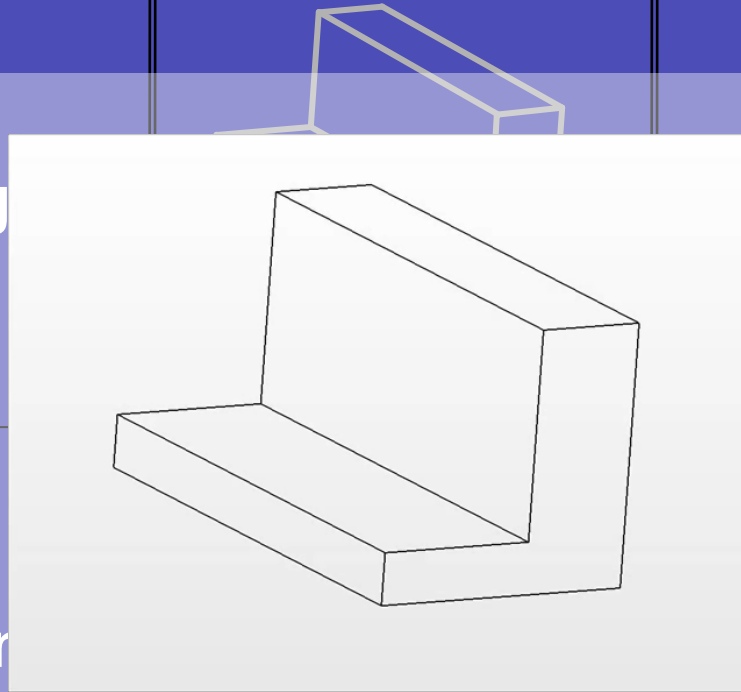
Haul-off Speed

Final Profile

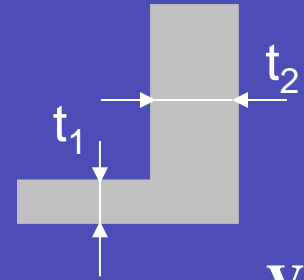


Length

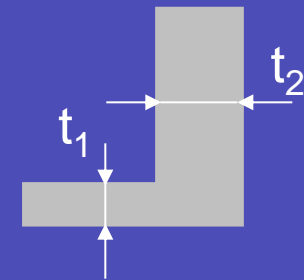
Thickness



V_3



$$\frac{V_3}{V_1} = \frac{V_3}{V_2}$$



$$\frac{V_3}{V_1} \neq \frac{V_3}{V_2}$$



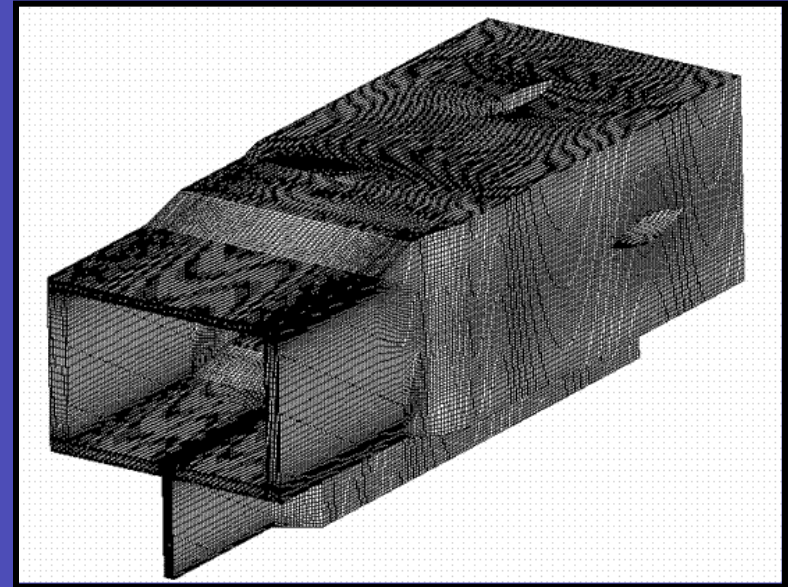


Constitutive equation

$$\eta(\dot{\gamma}, T) = F(\dot{\gamma} \times H(T)) H(T)$$

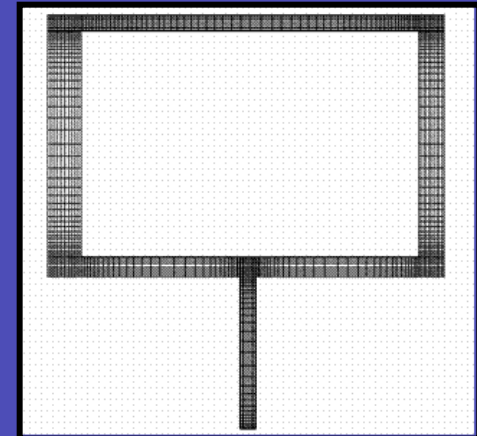
$$F(\dot{\gamma}) = \eta_{\infty} + \frac{\eta_0 - \eta_{\infty}}{(1 + (\lambda \dot{\gamma})^2)^{\frac{1-n}{2}}} \quad H(T) = \exp\left[\alpha\left(\frac{1}{T} - \frac{1}{T_a}\right)\right]$$

Mesh



Operating and thermal boundary conditions

Flow rate	20 kg/h
Melt inlet temperature	230 °C
Outer die walls temperature	230 °C
Inner (mandrel) die walls	Adiabatic





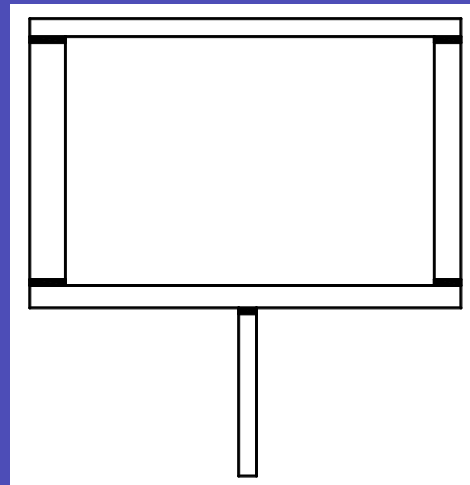
DieINI – Initial trial

Optimizations performed

DieL – Length optimisation

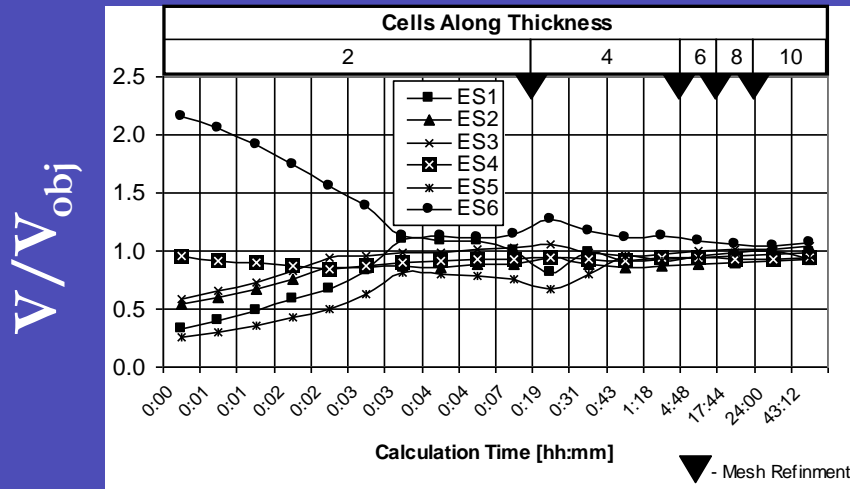
DieT – Thickness optimisation

DieLS – Length optimisation + Flow separators

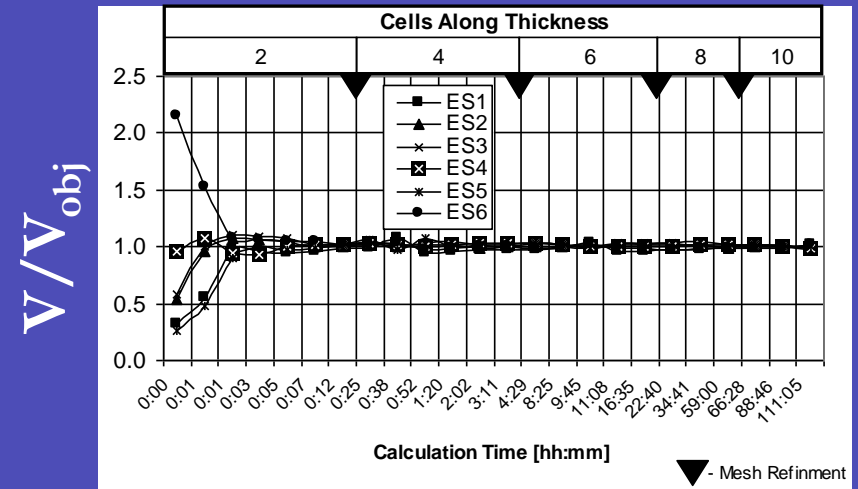




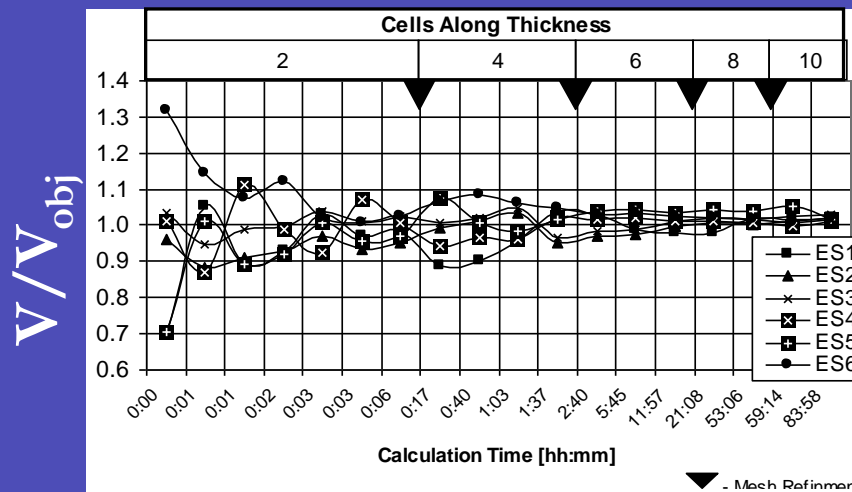
DieL



DieT

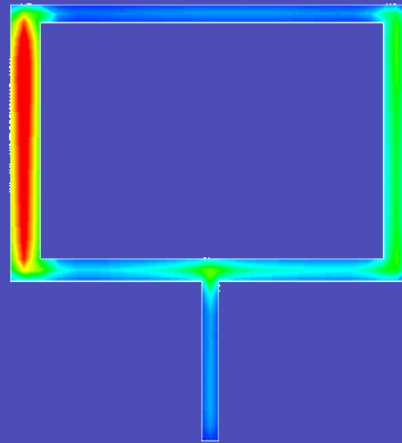


DieLS

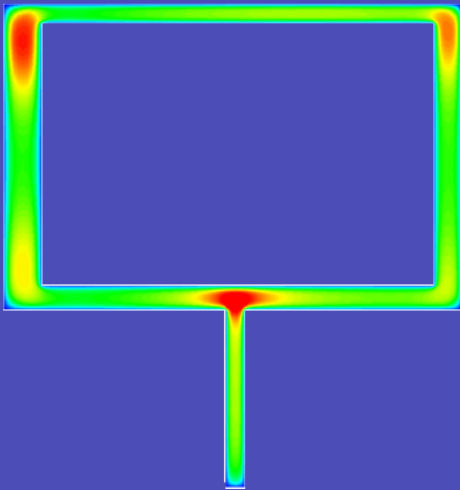




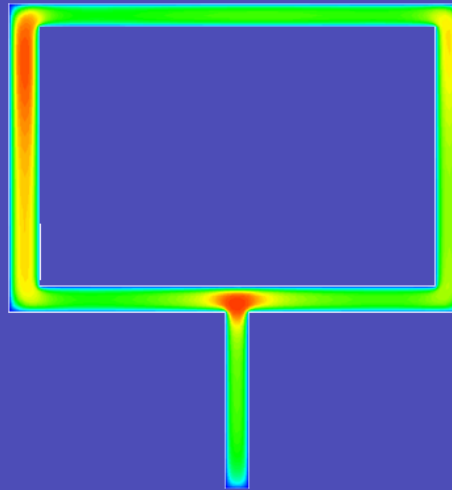
DieIni



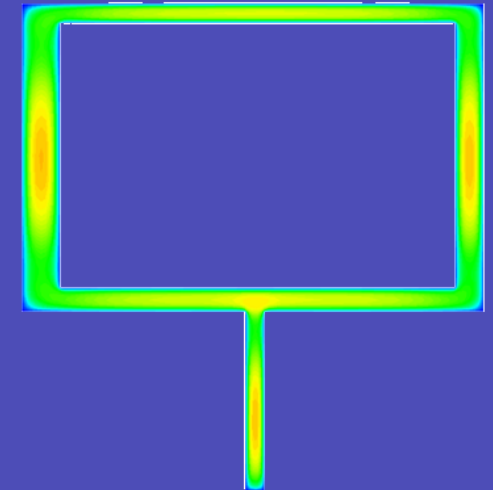
DieL



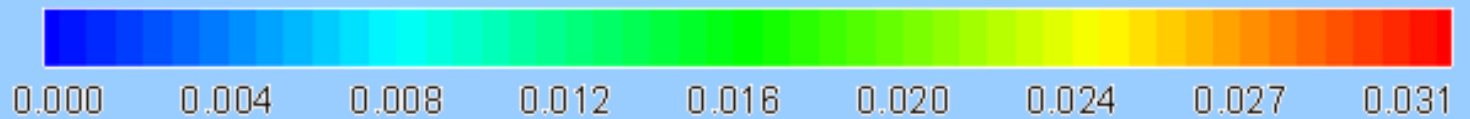
DieT



DieLS



Velocity [m/s]





DieIni

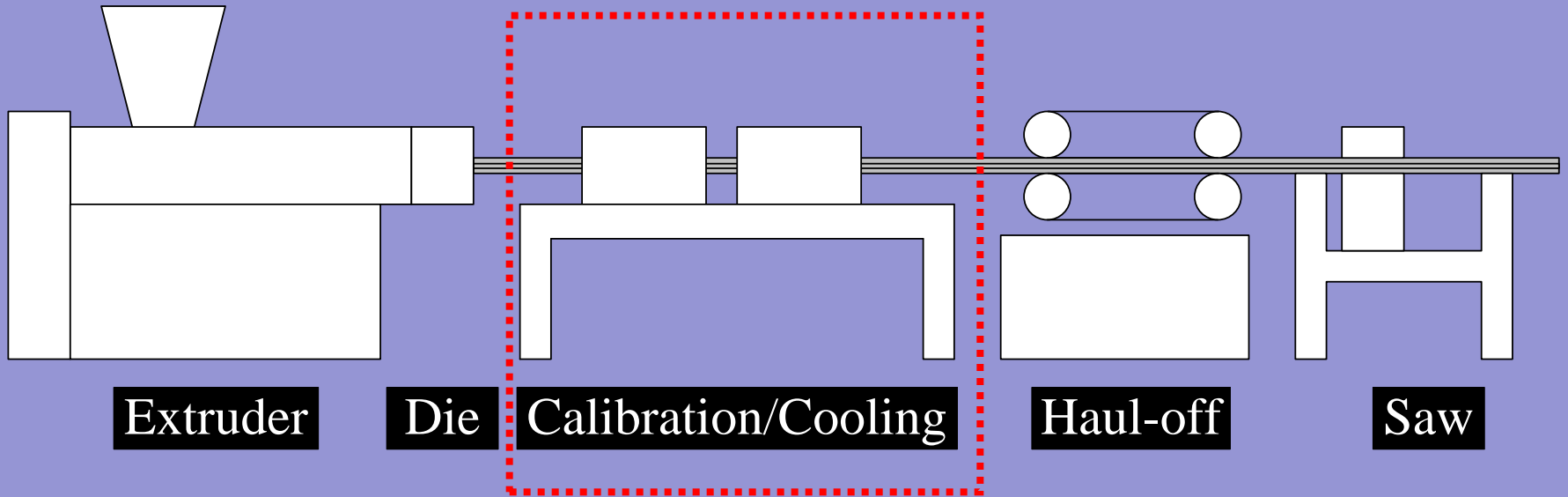


DieL

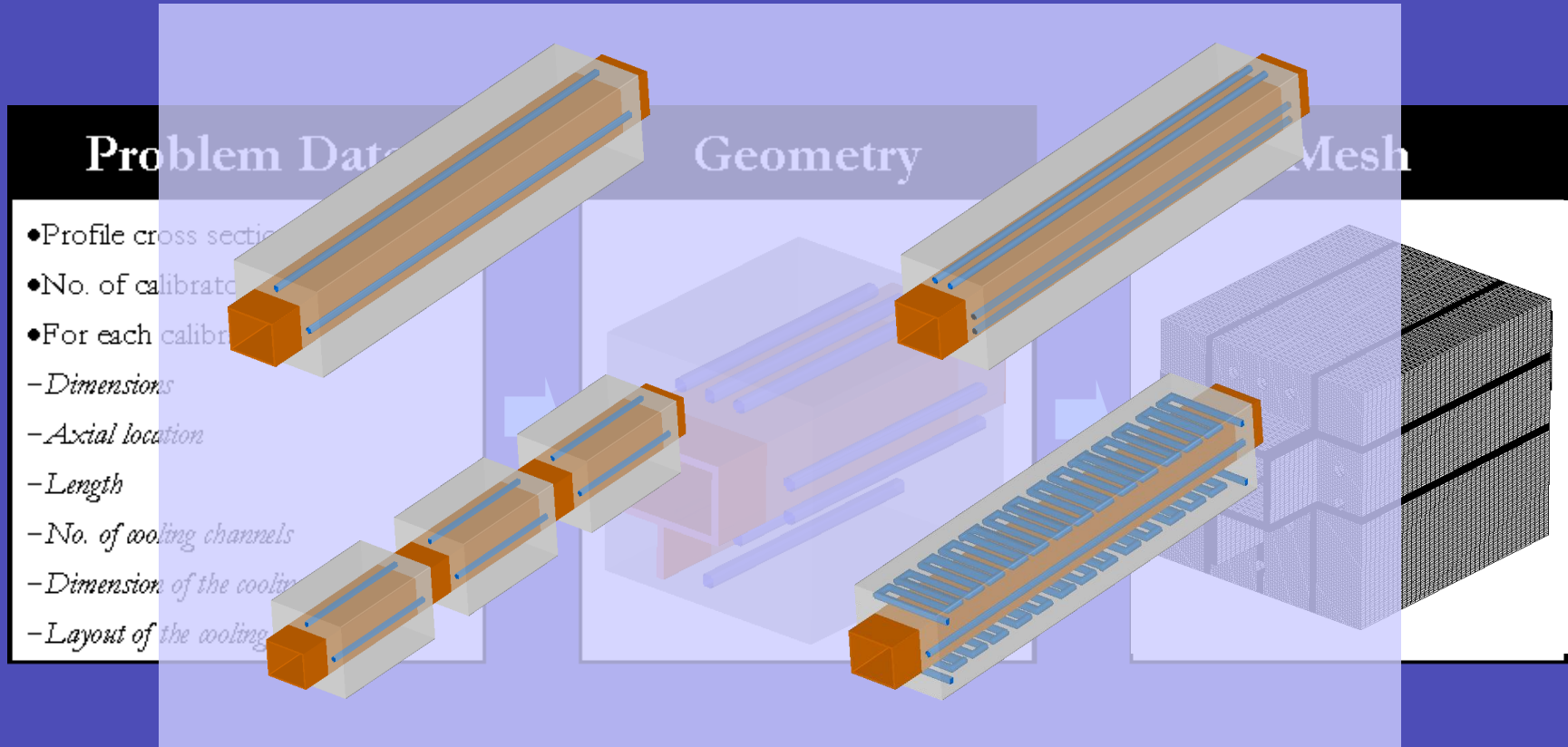


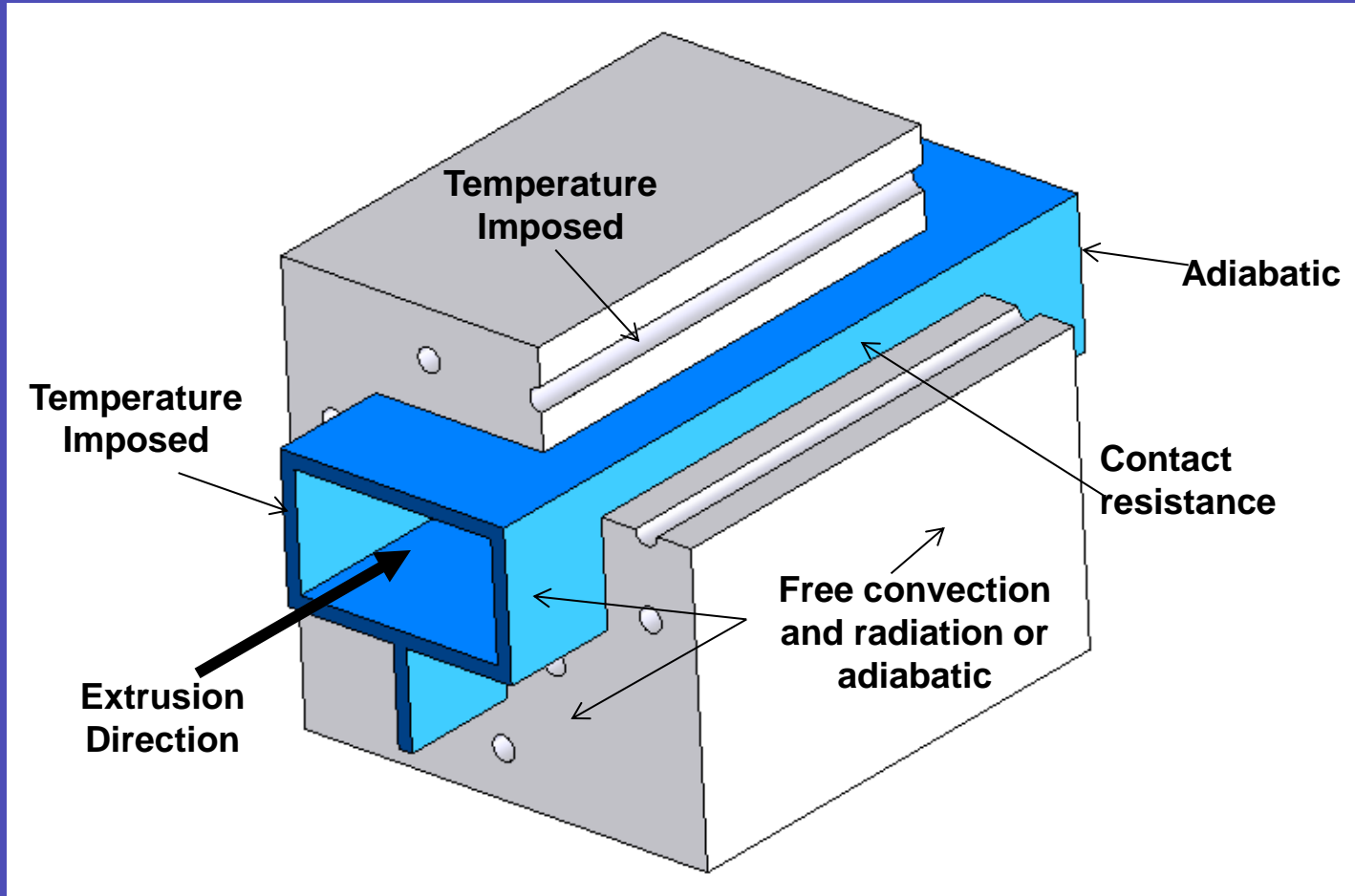
DieT





$$\bar{T} < T_s \quad \downarrow \quad \sigma_T$$







Polymer

$$\frac{\partial}{\partial x} \left(k_p \frac{\partial T_p}{\partial x} \right) + \frac{\partial}{\partial y} \left(k_p \frac{\partial T_p}{\partial y} \right) + \frac{\partial}{\partial z} \left(k_p \frac{\partial T_p}{\partial z} \right) - \rho_p c_p \frac{\partial}{\partial z} (w T_p) = 0$$

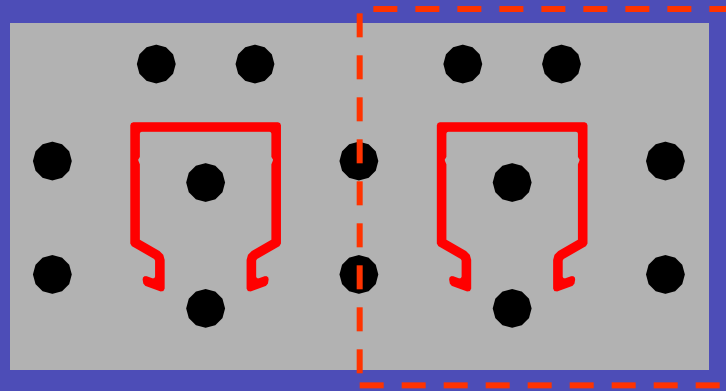
Calibrator

$$\frac{\partial}{\partial x} \left(k_c \frac{\partial T_c}{\partial x} \right) + \frac{\partial}{\partial y} \left(k_c \frac{\partial T_c}{\partial y} \right) + \frac{\partial}{\partial z} \left(k_c \frac{\partial T_c}{\partial z} \right) = 0$$

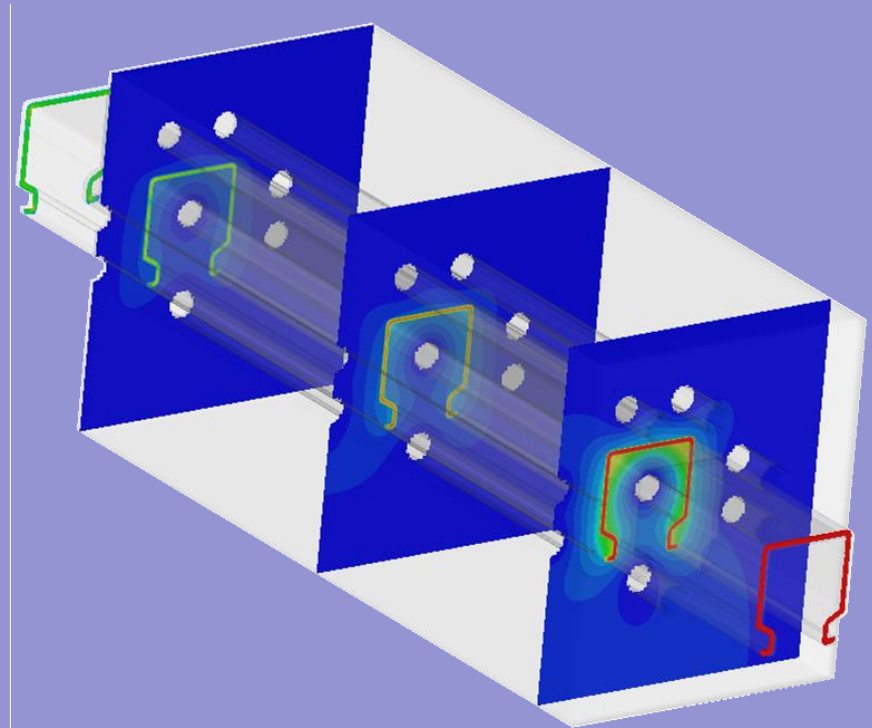
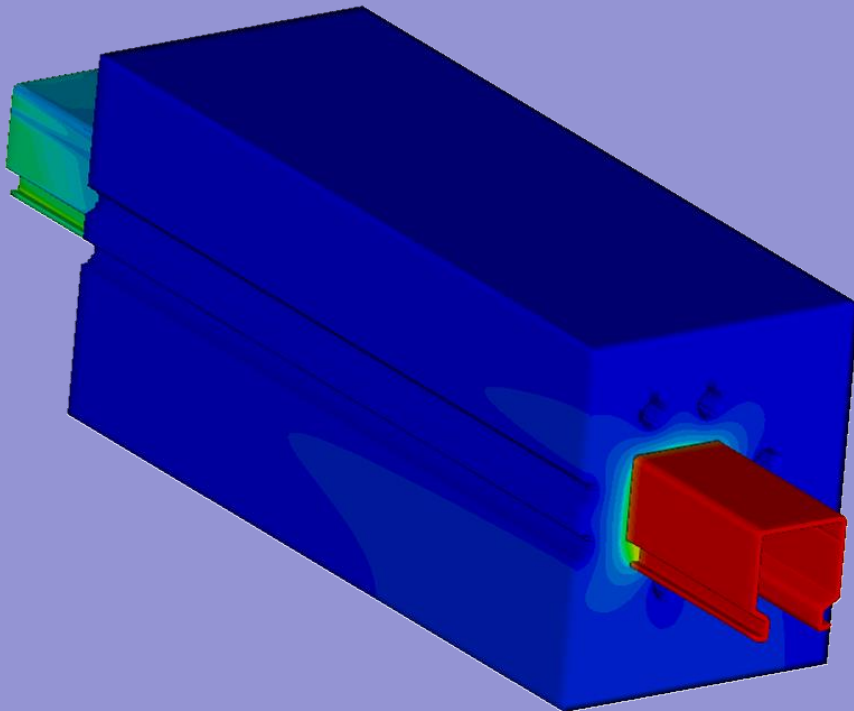
Polymer-calibrator interface

Contact Resistance

$$k_c \left(\frac{\partial T_c}{\partial n} \right)_{\text{interface}} = -k_p \left(\frac{\partial T_p}{\partial n} \right)_{\text{interface}} = h_i (T_p - T_c)_{\text{interface}}$$



3D Temperature field calculation (FVM)





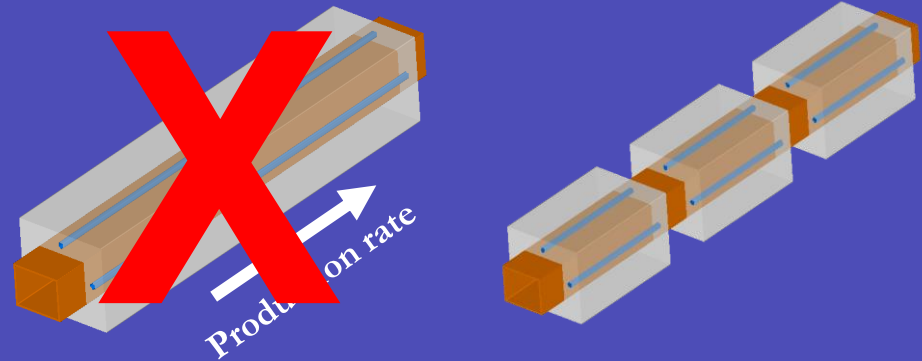
Influence of boundary conditions, process and geometrical parameters on the system performance (in terms of average temperature and temperature uniformity)

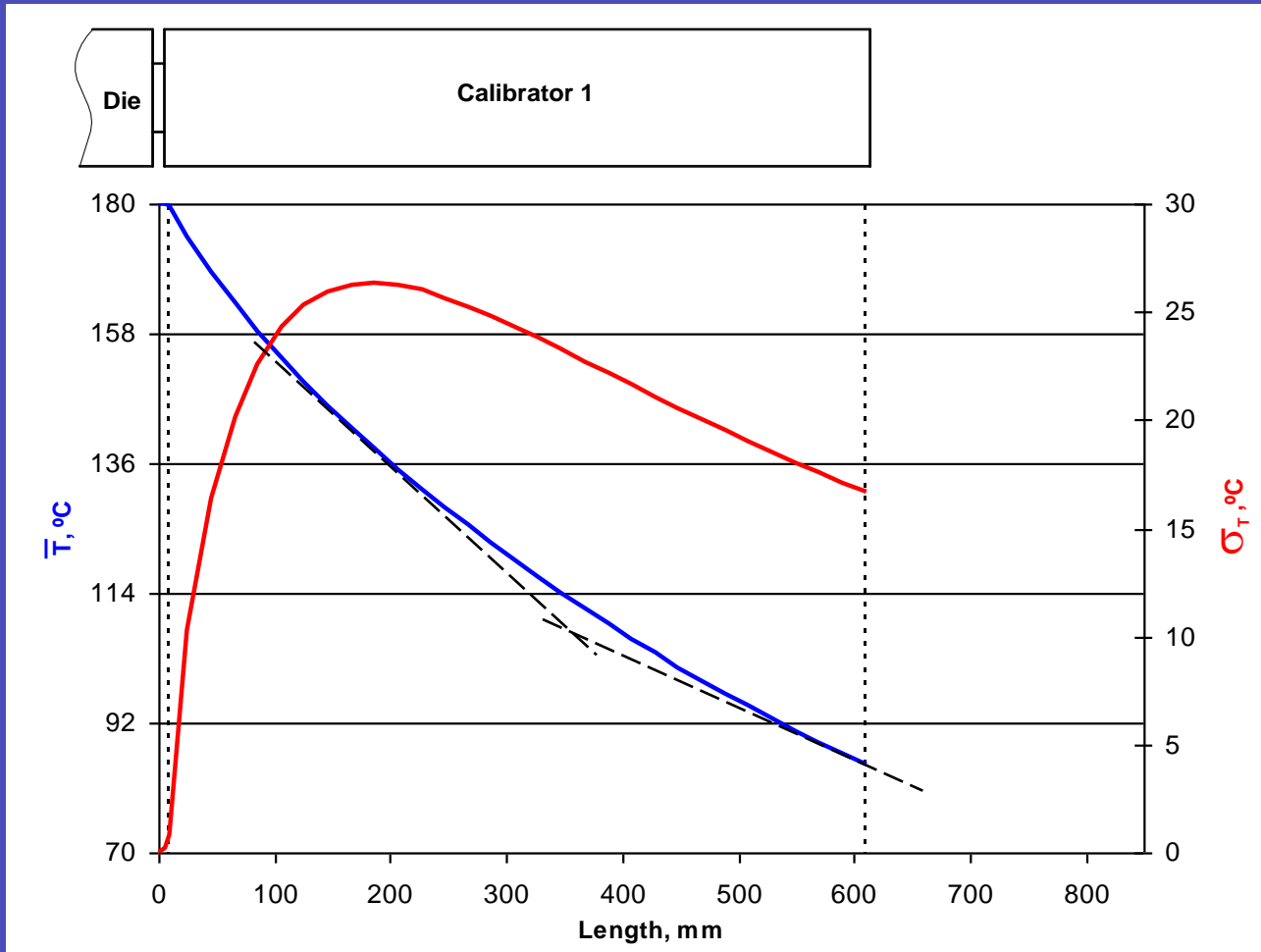
Conclusion:

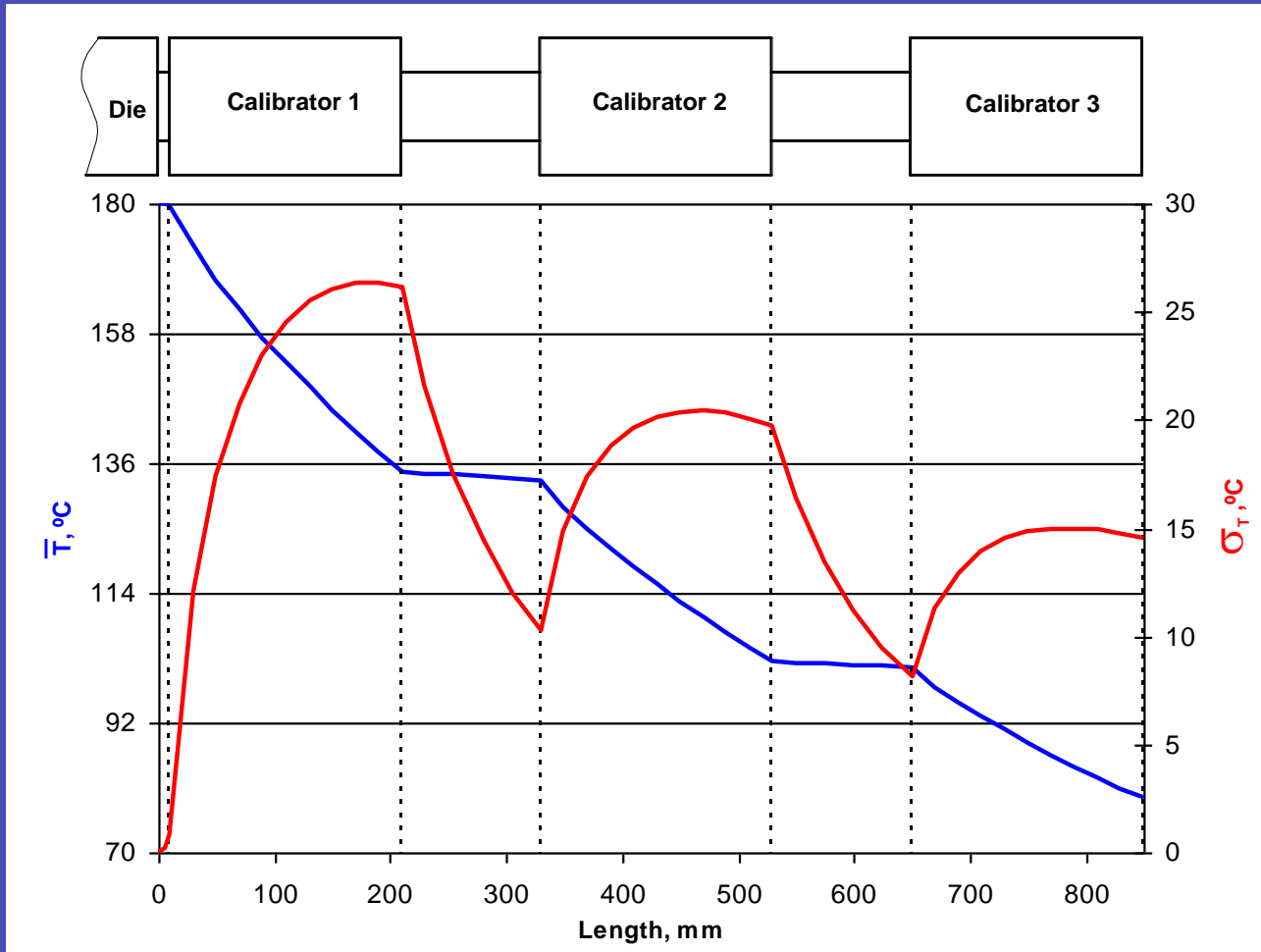
In general

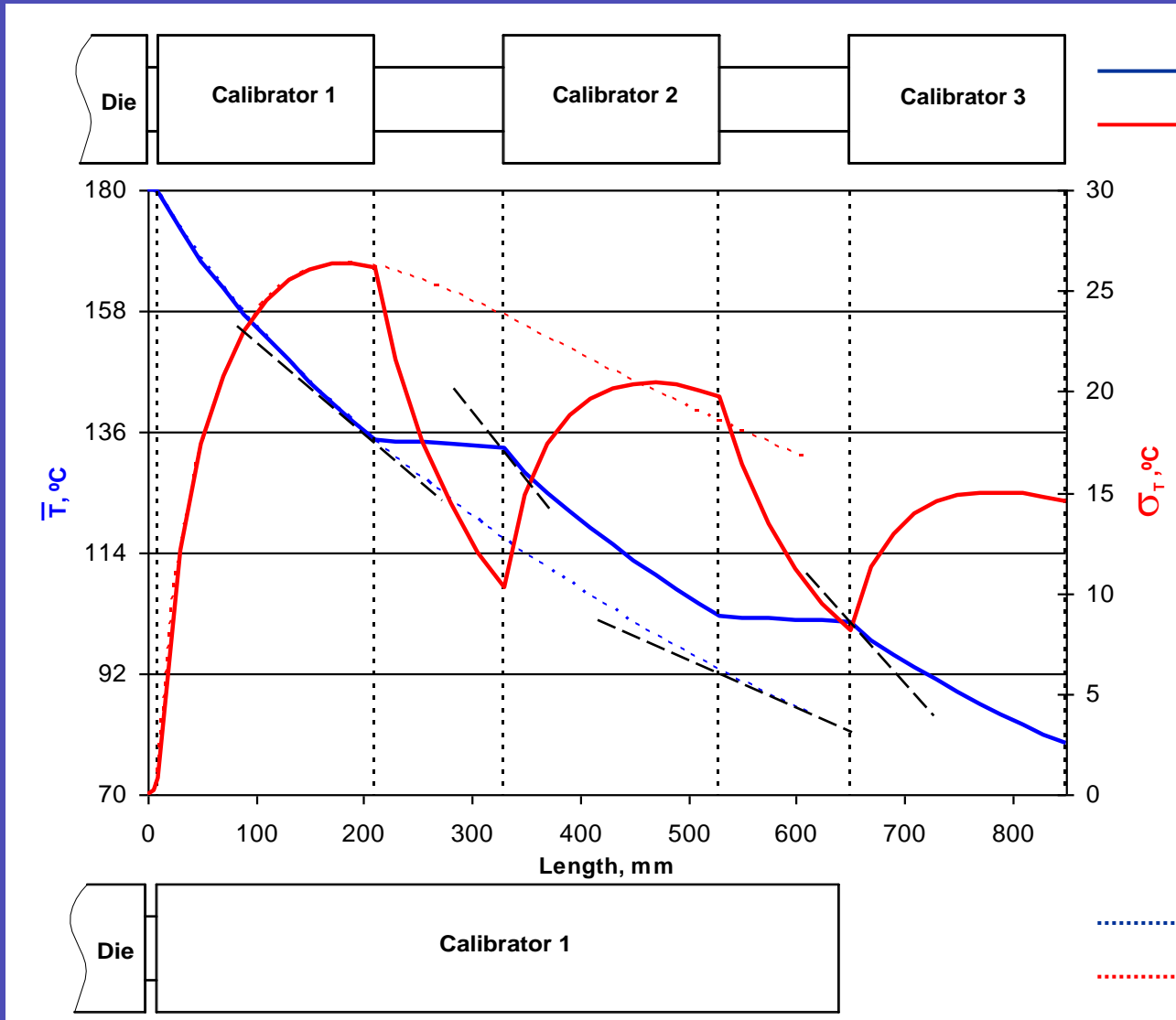
$$\downarrow \bar{T} \Rightarrow \uparrow \sigma_T$$

Exceptions





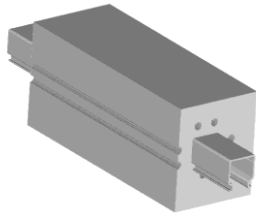




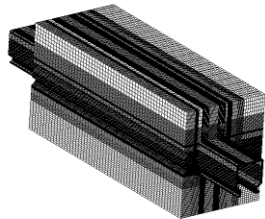


Input Data

Pre- Processor

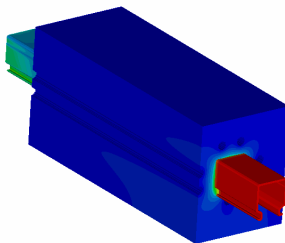


Geometry



Mesh

3D Temperature field calculation (FVM)



Temperature

Performance Evaluation

$$F_{obj} = \sum_{i=1}^n \alpha_i F_i$$

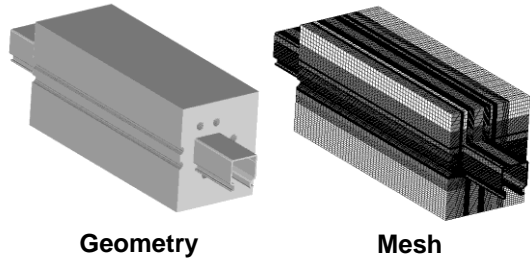
Optimisation: automatic generation of solutions (modification of the controllable geometrical parameters) until the optimum is reached





Input Data

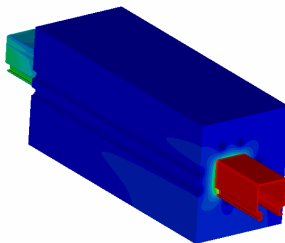
Pre-Processor



Geometry

Mesh

3D Temperature field calculation (FVM)



Temperature

Performance Evaluation

$$F_{obj} = \sum_{i=1}^n \alpha_i F_i$$

Optimisation: automatic generation of solutions (modification of the controllable geometrical parameters) until the optimum is reached

Temperature uniformity

$$\sigma_T = \sqrt{\frac{\sum_{i=1}^{n_f} (T_i - \bar{T})^2 A_i}{A_T}}$$

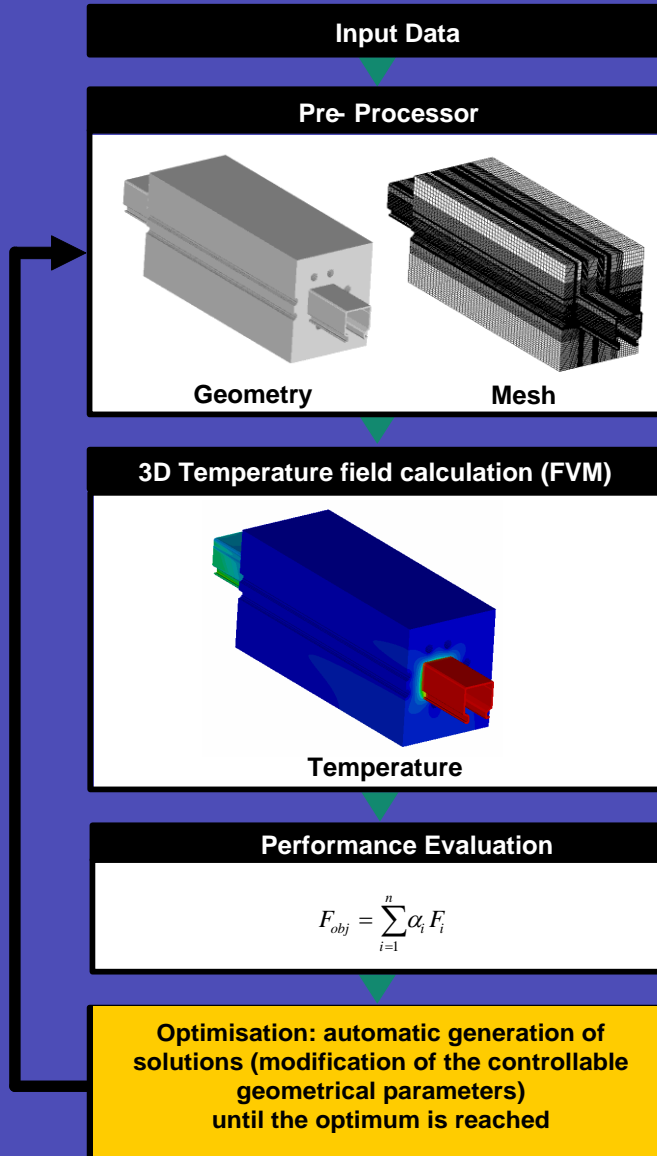
Cooling efficiency

$$\bar{T} = \frac{\sum_{i=1}^{n_f} T_i A_i}{A_T}$$

$$F_{obj} = K |\bar{T} - T_s| + \sigma_T$$

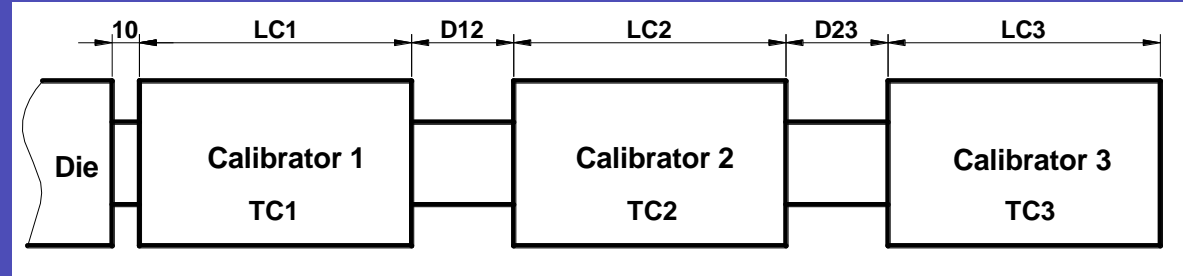
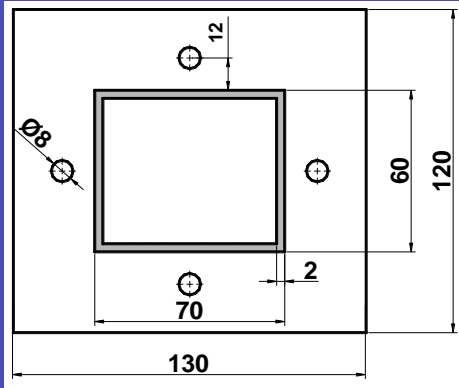
where:

$$\begin{cases} \bar{T} \leq T_s \Rightarrow K = 0 \\ \bar{T} > T_s \Rightarrow K = 1000 \end{cases}$$



Optimisation algorithm

Non-linear SIMPLEX method



Restrictions:

- Number of calibration/cooling units ≤ 3
- Total calibration length ($\sum LC_i$) ≤ 600 mm
- Total system length ($\sum LC_i + \sum D_{ij} + 10$) ≤ 850 mm
- Cooling Fluid Temperature $TC_i \in [10^\circ\text{C}, 26^\circ\text{C}]$



General conditions for the simulations

Processing conditions

$$v_p = 2 \text{ m/min}$$

$$T_m = 180 \text{ }^\circ\text{C}$$

$$T_f = 18 \text{ }^\circ\text{C}$$

$$T_s = 80 \text{ }^\circ\text{C}$$

Materials Properties

$$K_p = 0.18 \text{ W/mK}$$

$$K_c = 14 \text{ W/mK}$$

$$\rho_p = 1400 \text{ kg/m}^3$$

$$c_p = 1000 \text{ J/kgK}$$

Boundary conditions

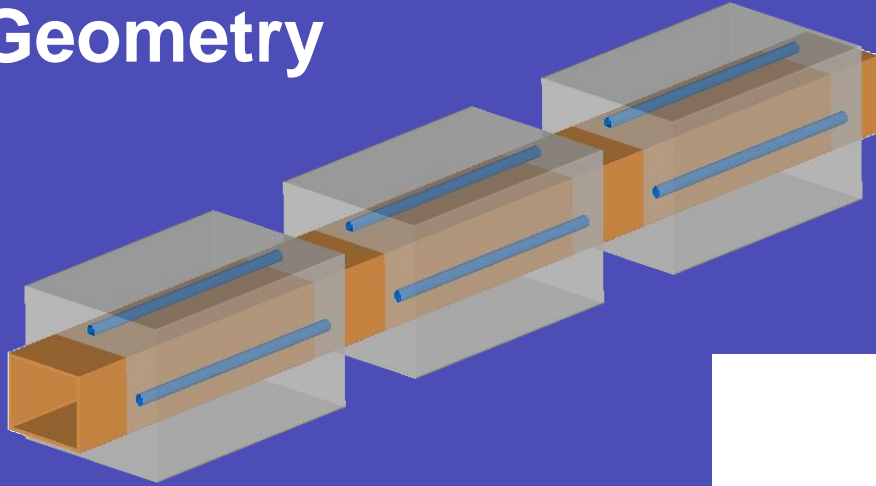
Annealing zones: free convection and radiation

Polymer-calibrator interface: contact resistance

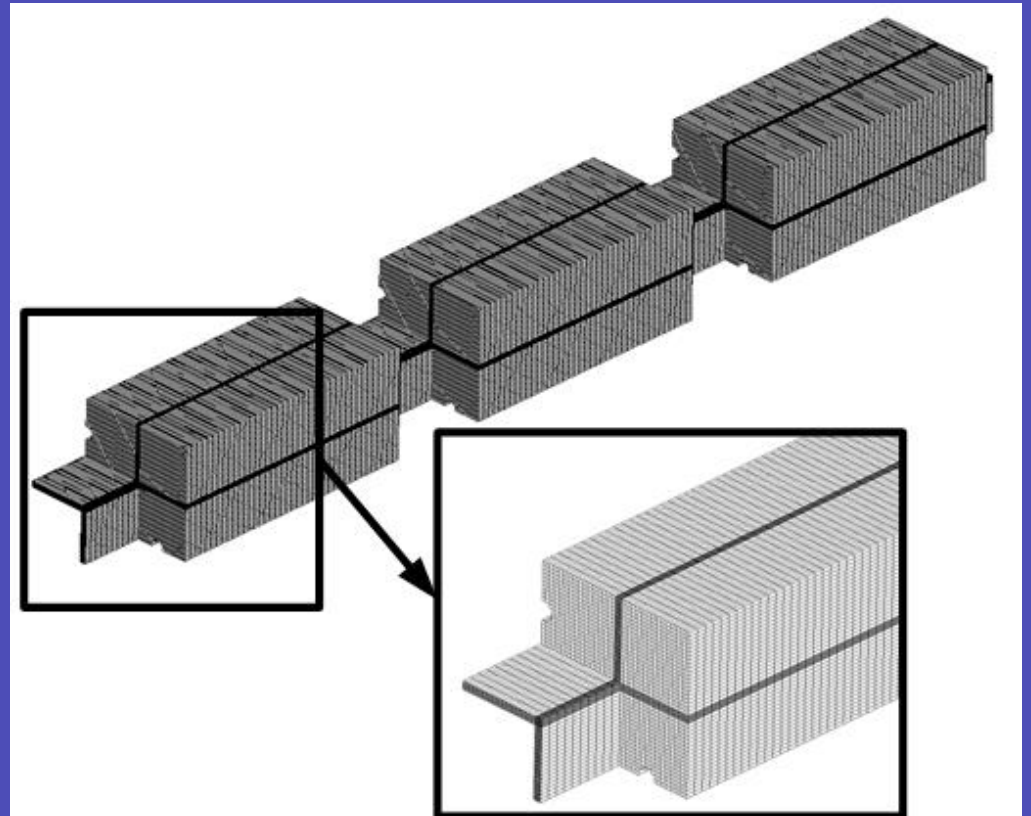
$$(h_i = 425 \text{ W/m}^2\text{K})$$

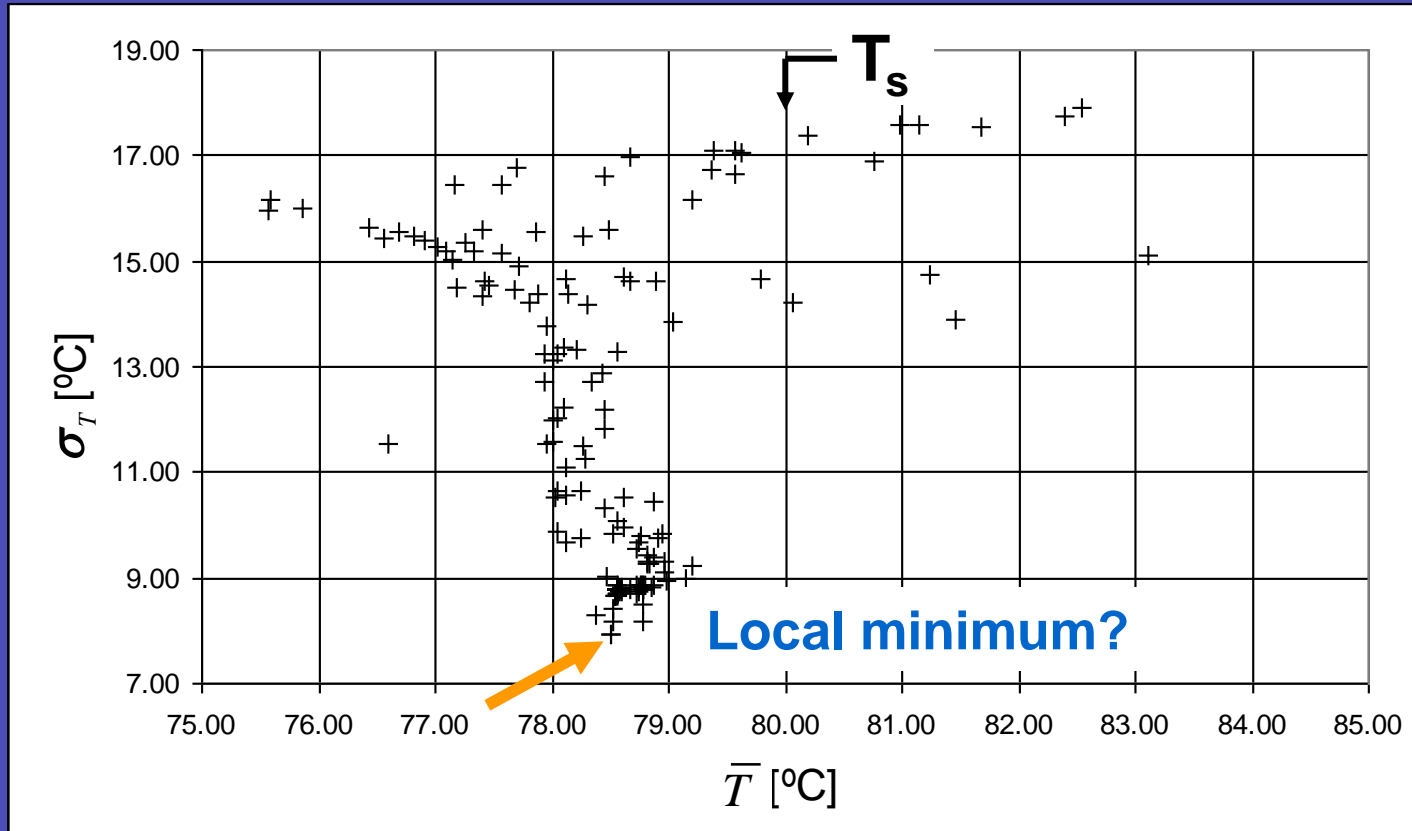


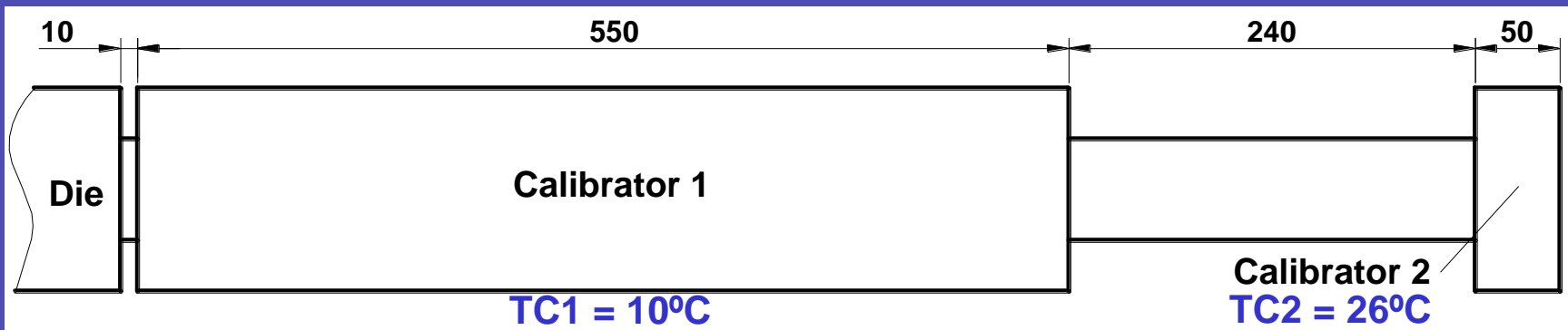
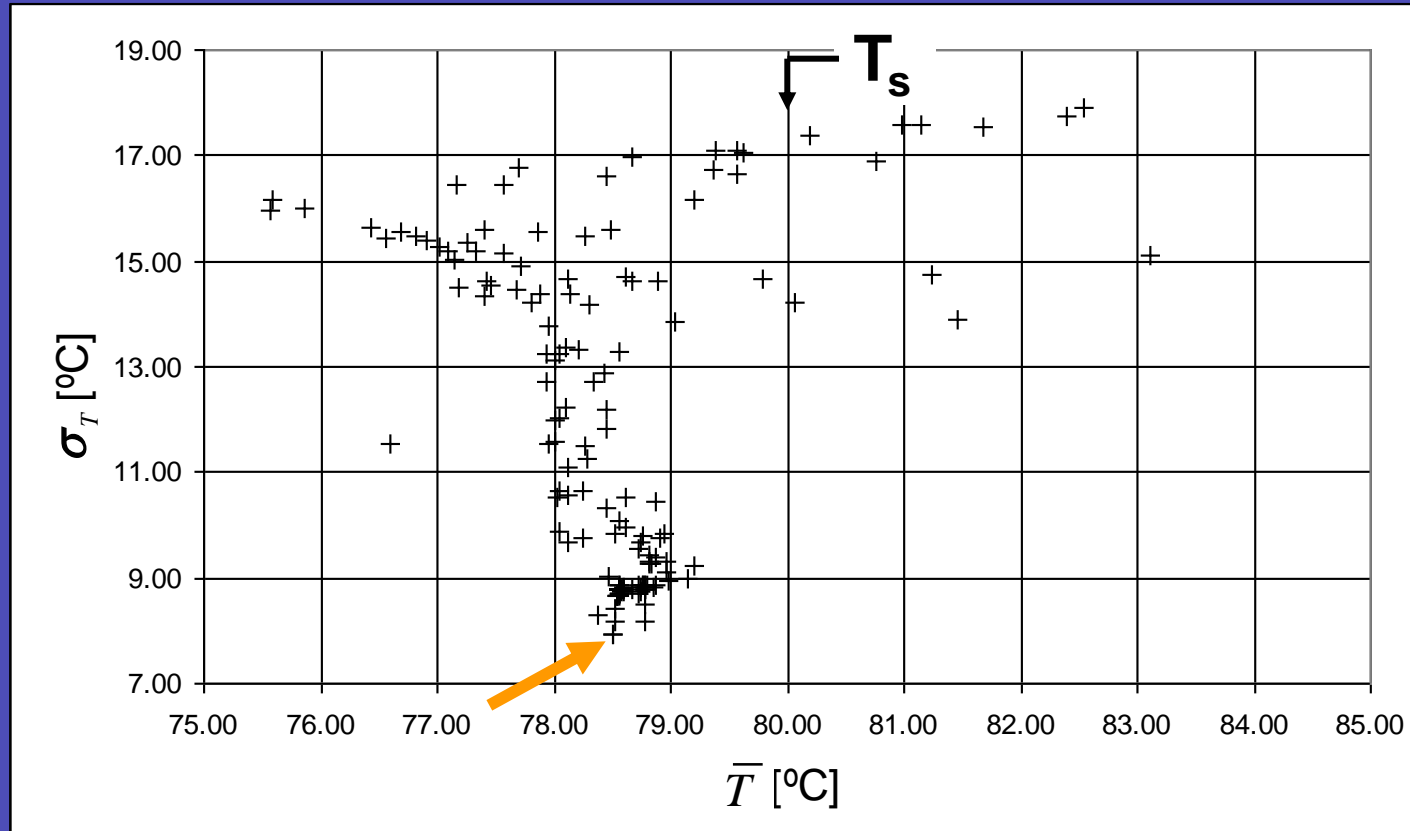
Geometry



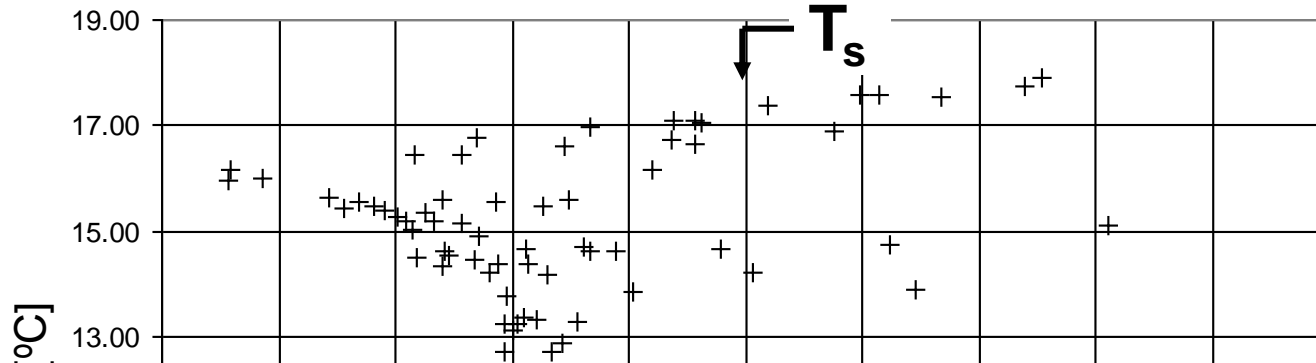
Mesh





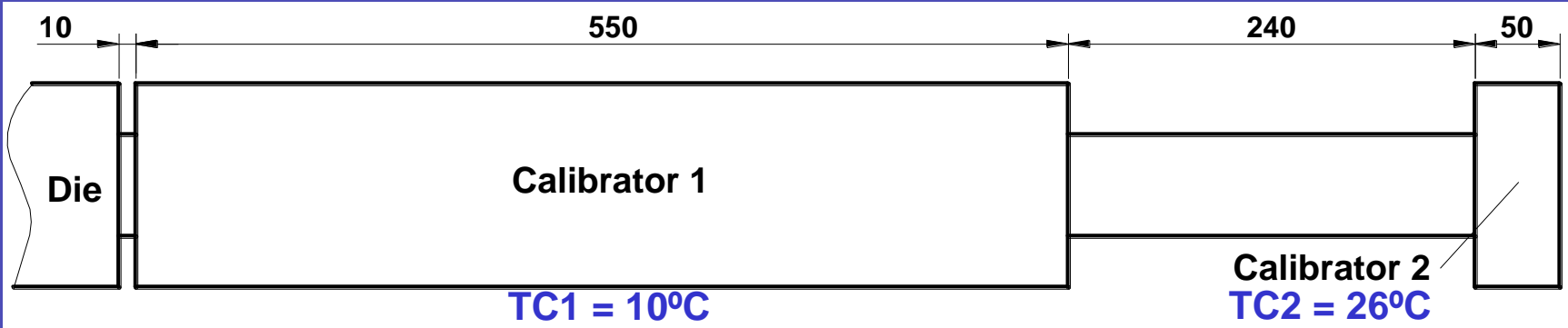


Calibrators - Case Study



Geometry	\bar{T} [°C]	σ_T [°C]
One Calibrator (TC=18°C)	84.9	16.6
Optimum Solution	78.5	7.9

- 52.4%





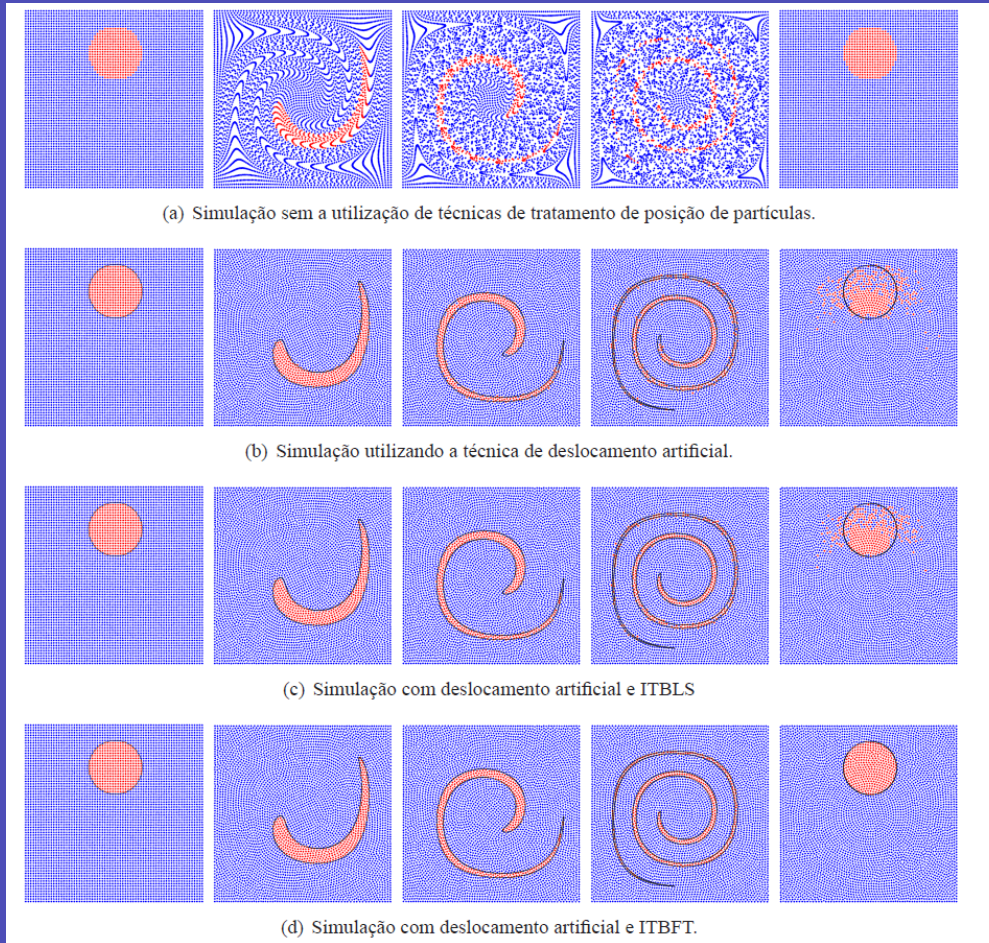
- Implementation of the wall Slip and free-surface boundary conditions (**L.L. Ferrás**, Post-doctoral project);
- Development of unstructured numerical modelling code (**N.D. Gonçalves**, PhD project);
- Implementation of viscoelastic constitutive equations in an unstructured modelling code (**S. Reddy**, MSc Eurheo project);
- Prediction of thermal induced stresses in calibration in **OpenFOAM** (**S. Reddy**, Research Project);
- Development of high order interpolation schemes (**R. Costa**, FCT Research Project, DMAT);
- Portability and Performance in Heterogeneous Many-core Systems (**R. Ribeiro**, PhD Project, DI) - **OpenFOAM**;



- **Development of multiscale modelling approaches** (**S.T. Mould**, PhD Project);
- **Development of ISPH numerical modelling code** (**D.F. Cordeiro**, PhD/Cooperation Project, USP);
- **Development of FSI methodologies for the design of extrusion dies in **OpenFOAM**** (**M.R. Moosavi**, Post-doctoral grant);
- **Modelling the cooling stage in profile extrusion using **OpenFOAM**** (**R. Ananth**, PhD project, MIT+Soprefa);
- **Design of a new generation of car washing machines** (**M. Sabet**, PhD project, MIT+Petrotec);
- **Characterisation of the heat transfer coefficient at the polymer-metal interface in profile cooling** (**F. Araújo**, FCT Research Project);

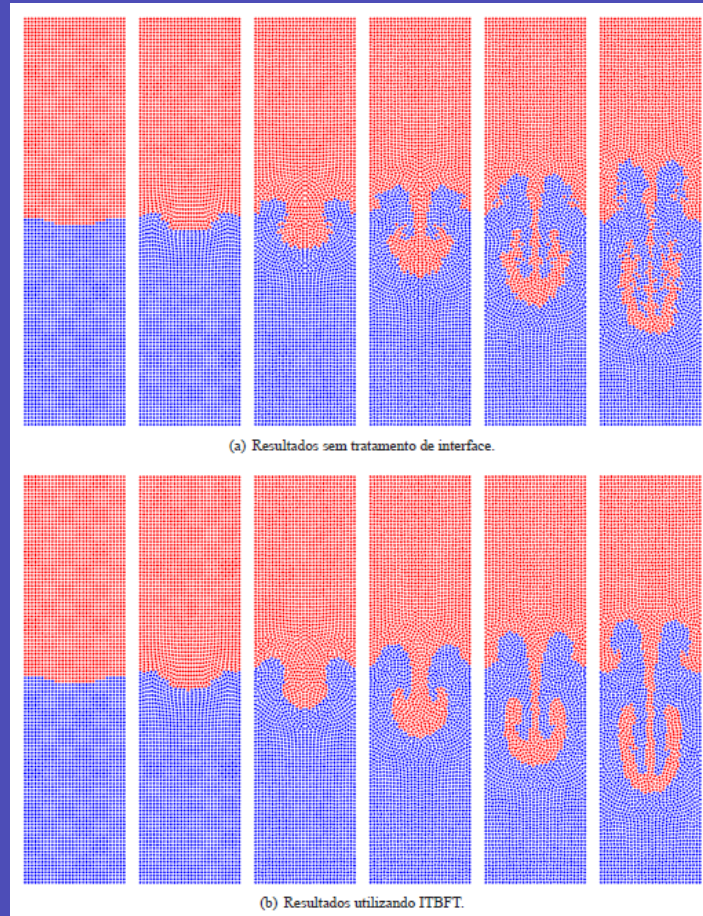


- Development of ISPH numerical modeling code (D.F. Cordeiro, PhD/Cooperation Project, USP);





- Development of ISPH numerical modelling code (D.F. Cordeiro, PhD/Cooperation Project USP);





- Development of ISPH numerical modeling code (D.F. Cordeiro, PhD/Cooperation Project, USP);

